

# Enhanced hydrogen reaction kinetics of nanostructured Mg-based composites with nanoparticle metal catalysts dispersed on supports

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## Abstract

Hydrogen reaction kinetics of nanocrystalline MgH<sub>2</sub> co-catalyzed with Ba<sub>3</sub>(Ca<sub>1+x</sub>Nb<sub>2-x</sub>)O<sub>9-δ</sub> (BCN) proton conductive ceramics and nanoparticle bimetallic catalyst of Ni/Pd dispersed on single wall carbon nanotubes (SWNTs) support has been investigated. The nanoparticle bimetallic catalysts of Ni/Pd supported by SWNTs were synthesized based on a novel polyol method using NiCl<sub>2</sub>·6H<sub>2</sub>O, PdCl<sub>2</sub>, NaOH and ethylene glycol (EG). The nanostructured Mg composites co-catalyzed with BCN and bimetallic supported catalysts exhibited stable hydrogen desorption capacity of 6.3–6.7 wt.% H<sub>2</sub> and the significant enhancement of hydrogen desorption kinetics at 230–300 °C in comparison to either non-catalyzed MgH<sub>2</sub> or the nanocomposite of MgH<sub>2</sub> catalyzed with BCN.

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**Keywords:** Hydrogen storage materials; Polyol method; Ni/Pd nanoparticle catalyst; Magnesium hydride; Proton conductive ceramic catalyst

## 1. Introduction

Magnesium hydride having a high hydrogen storage capacity of 7.6 wt.% is considered as one of the most interesting alternatives for the reversible storage of hydrogen. However, the major problem of magnesium as a rechargeable hydrogen carrier system is its slow reaction rate and high sorption temperature. To overcome this problem, metallic catalysts such as Pd, Ni, V, Ti, Mn and Fe have been added to nanocrystalline magnesium for a better H<sub>2</sub>-dissociation at the surface [1,2]. Recently Hanada et al. have reported the catalytic effect of nanoparticle Ni on hydrogen storage properties of MgH<sub>2</sub> [3,4]. The nanosized Ni doping significantly decreased the activation energy for hydrogen desorption by surface activation, resulting in 90% of hydrogen desorption within 100 min at 163 °C. Kojima et al. have reported that nanocomposite MgH<sub>2</sub> catalyzed with nano-Ni/Al<sub>2</sub>O<sub>3</sub>/C desorbed 4.9–5.8 wt.% H<sub>2</sub> at 423–473 K [5]. Gutfleisich et al. have reported that hydrogen desorption temper-

ature is reduced significantly to less than 140 °C when MgH<sub>2</sub> is co-milled with 0.5 wt.% PdOH<sub>2</sub>O and 5 at.% or 10 at.% Ni [6]. In addition, Gutfleisich et al. have also reported a Mg–1 wt.% Ni–0.2 wt.% Pd alloy produced via induction melting with consequent reactive milling exhibited 41 kJ/mol for absorption and 110 kJ/mol for the desorption reaction, indicating excellent hydrogen absorption/desorption kinetics [7]. Therefore, nano-Ni/Pd catalyst uniformly dispersed on nanocrystalline MgH<sub>2</sub> can be considered to exhibit very attractive catalytic effect on enhancing hydrogen sorption kinetics.

In another approach, transition metal oxides such as TiO<sub>2</sub>, V<sub>2</sub>O<sub>5</sub>, CuO, Mn<sub>2</sub>O<sub>3</sub>, Cr<sub>2</sub>O<sub>3</sub>, Fe<sub>3</sub>O<sub>4</sub>, and Nb<sub>2</sub>O<sub>5</sub>, etc. have been investigated as potential catalysts on the sorption behavior of nanocrystalline Mg-based systems [3,8]. Recently, Yoo et al. have reported the catalytic effect of proton conductive ceramics on enhancing hydrogen desorption kinetics of nanostructured magnesium hydrides [9,10]. After milling MgH<sub>2</sub>–Ba<sub>3</sub>(Ca<sub>1+x</sub>Nb<sub>2-x</sub>)O<sub>9-δ</sub> (BCN) composite, the nanostructured composite showed much enhanced desorption kinetics, increased desorption plateau pressure, and decreased hysteresis,  $\ln(P_{\text{abs}}/P_{\text{des}})$ , indicating not only ameliorate desorption kinetics but also lower temperature desorption in comparison to pure MgH<sub>2</sub>.

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Therefore, in this work, the hydrogen reaction kinetics of nanocrystalline  $\text{MgH}_2$  co-catalyzed with  $\text{Ba}_3(\text{Ca}_{1+x}\text{Nb}_{2-x})\text{O}_{9-\delta}$  (BCN) proton conductive ceramics and nanoparticle bimetallic catalysts of Ni/Pd dispersed on single wall carbon nanotubes (SWNTs) support has been investigated.

## 2. Experimental procedures

Magnesium hydride ( $\text{MgH}_2$ ) powder was purchased from Alfa-Aesar (98% purity) and mechanically milled under argon by using a Spex 8000 high energy mill for 18 h to prepare nanostructured  $\text{MgH}_2$ . The ball to powder ratio was 10:1.

BCN catalyst ( $\text{Ba}_3(\text{Ca}_{1+x}\text{Nb}_{2-x})\text{O}_{9-\delta}$ ,  $x=0$ ) [11] was prepared from polymeric precursors by the Pechini method [12]. The starting materials of barium carbonate dissolved in nitric acid solution, calcium carbonate dissolved in nitric acid solution, and ammonium citric solution converted from ammonium niobate oxalate hydrate were mixed with a stoichiometric amount of citric acid. The resulting solution was stirred for about 1 h on a hot plate and the temperature was stabilized at 70 °C. The mixture was heated to 90 °C, at which point ethylene glycol was added at a mass ratio of 40:60 with respect to citric acid. The temperature was maintained constant at 160 °C for resin formation and thermal decomposition. The precursor powders were then calcined at 700 °C for 4 h and again heat-treated at 1000 °C for 1 h as the final step for the synthesis of BCN single phase.

The nanoparticle Ni/Pd catalysts (Ni:Pd = 10:1 and 2:1 in molar ratio) supported on SWNTs (Ni/Pd:SWNT = 1:1 weight ratio) also having catalytic effect on enhancing kinetics of hydrogen storage materials were prepared based on a novel polyol method developed by Bock et al. [13] for preparing Pt/Ru nanoparticles. In this method, precursor salts of  $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$  (Sigma–Aldrich, PeagentPlus) and  $\text{PdCl}_2$  (Sigma–Aldrich, 99.9%) were dissolved in ethylene glycol containing 0.2 M NaOH. The solutions were stirred for 30 min in air at room temperature, subsequently heated under reflux to 160 °C for 3 h, and then cooled in air. Appropriate aliquots of the colloidal solutions were mixed with single wall carbon nanotubes (Microtechnano, SWNTs purity 92 wt.%, amorphous carbon 6 wt.%, ash 2 wt.%, surface area 640  $\text{m}^2/\text{g}$ ) in a large and open beaker for up to 24 h, resulting in the deposition of the Ni/Pd colloids on the SWNTs. The SWNTs-supported Ni/Pd catalysts were then filtered, washed with water, and dried at 100 °C in air for 1 h.

The nanocrystalline composites of  $\text{MgH}_2$  containing BCN catalyst were prepared by milling a mixture of 18 h milled  $\text{MgH}_2$  and 2 wt.% of BCN for additional 2 h. The final co-catalyzed  $\text{MgH}_2$  nanocomposites containing the supported Ni/Pd catalysts as well as BCN were prepared by milling a mixture of the milled  $\text{MgH}_2$ –BCN composite and the SWNTs-supported Ni/Pd catalysts for additional 20 min.

Thermodynamics and kinetics of the nanostructured  $\text{MgH}_2$  composites were determined by a Sievert-type sorption analyzer (Hy-Energy, PCT Pro2000). The surface morphology, microstructure, surface oxidation state and phase of the as-milled  $\text{MgH}_2$  and the supported catalysts were determined by using scanning electron microscopy (SEM), transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS) and X-ray diffraction on a Bruker's D8 Diffractometer. The crystallite size was also obtained by a TOPAS program (Bruker). The dehydrogenation behavior of the nanocomposites with catalysts was studied by differential scanning calorimetry (DSC 2920, TA instruments). The milled nanocomposite sample of 4 mg was placed in an aluminum pan, and a lid was crimped onto the pan in dry box filled with argon. The pan was then placed in the sample cell of the DSC module. The temperature of the DSC module was equilibrated at 50 °C and then increased at a rate of 1–20 °C/min under a  $\text{N}_2$  gas purge up to 500 °C.

## 3. Results and discussion

### 3.1. Structural characterization of mechanically milled $\text{MgH}_2$ and synthesized catalysts

Fig. 1 shows the X-ray diffraction patterns of the composites: (a) pure  $\text{MgH}_2$  as received, (b)  $\text{MgH}_2$  milled for 18 h, (c) synthe-

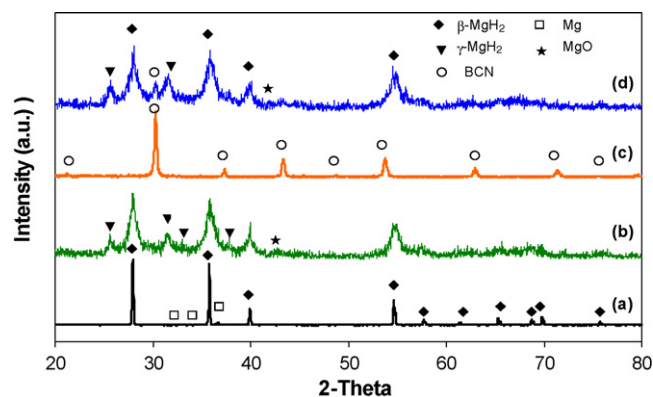


Fig. 1. X-ray diffraction patterns of the composites: (a) pure  $\text{MgH}_2$  as received, (b)  $\text{MgH}_2$  milled for 18 h, (c) BCN catalyst and (d)  $\text{MgH}_2$ –2 wt.% BCN nanocomposite milled for additional 2 h.

sized BCN catalyst and (d)  $\text{MgH}_2$ –2 wt.% BCN nanocomposite milled for additional 2 h. As shown in Fig. 1(a) and (b), the high energy milling of as-received  $\text{MgH}_2$  for 18 h increased the diffraction peak line widths, indicating that the high energy milling reduced the average crystallite size present in the original  $\beta$ - $\text{MgH}_2$  material and/or increased its microstructural strain, and induced the phase transformation from  $\beta$ - $\text{MgH}_2$  tetragonal phase and  $\gamma$ - $\text{MgH}_2$  orthorhombic phase. Fig. 1(c) shows a well crystallized cubic perovskite structure of BCN single phase. As shown in Fig. 1(d), the additional milling of the mixture of 18 h milled  $\text{MgH}_2$  and BCN catalyst for 2 h kept the BCN phase, indicating that the proton conductor exists on the surface of  $\text{MgH}_2$  particles and that surface inter-diffusion between  $\text{MgH}_2$  and BCN may cause the formation of Ba, Ca and Nb-rich reacted zone as hydroxides or even hydrides on the surface of  $\text{MgH}_2$  as described in Ref. [10].

SWNTs-supported Ni/Pd catalysts having two different molar ratios of Ni/Pd = 10/1 and 2/1 were synthesized by the polyol method using ethylene glycol (EG)–NaOH. As for a supporting material for the deposition of metal nanocatalysts, SWNTs was used because it was reported that SWNTs can act as catalysts to improve the hydrogen absorption and desorption properties of metallic catalyst-doped hydrides [14,15]. It was also reported that the nanotube length decreases with increasing ball milling time [16]. In order to prevent the thorough destruction of SWNTs during the high energy milling, a short milling time of 20 min was applied for mixing the milled  $\text{MgH}_2$ –BCN composite and the SWNTs-supported Ni/Pd catalysts in this study. However, it should be noted that the high surface area carbon as a supporting material may provide a similar beneficial effect on enhancing hydrogen sorption kinetics and the direct observation of SWNTs in the milled composites as a function of milling time has to be done to confirm the effect of mechanically milled SWNTs in the composites.

Ethylene glycol is an alcohol and is readily oxidized to act as a reducing agent for the Ni and Pd precursor salts. The detailed suggested mechanism was described in literature [13]. The addition of NaOH into the EG system accelerates the reduction of metal ions to metal nanoparticles even at room tempera-

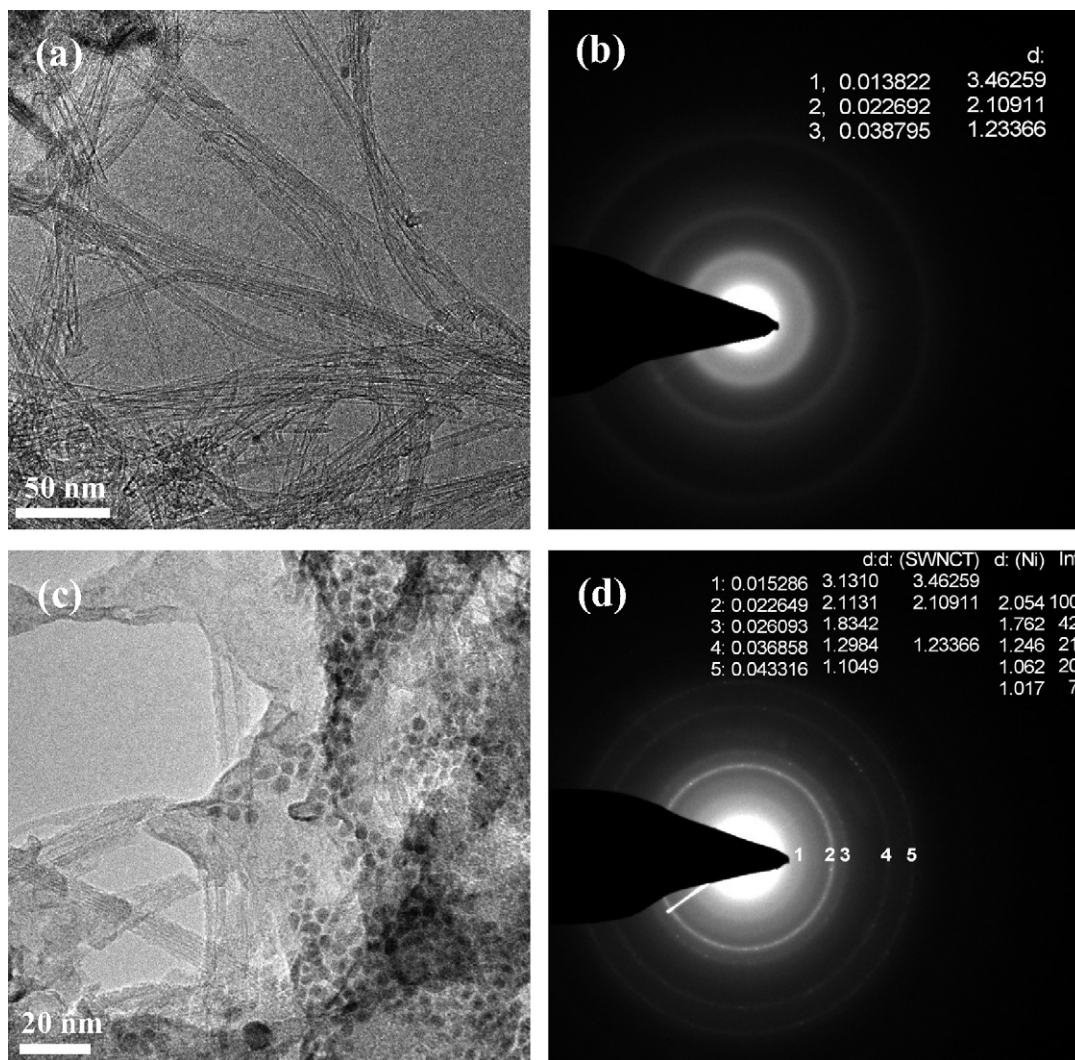


Fig. 2. Transmission electron micrographs and electron diffraction patterns of (a) and (b) SWNT and (c) and (d) supported Ni catalysts.

ture without the need for external reducing agent and decreases the particle size [17]. The formation of Ni metal nanoparticles by chemical method is known to be very difficult because nickel is easily oxidized [18]. The X-ray diffraction patterns and XPS spectra of SWNTs-supported Ni/Pd catalysts prepared in ethylene glycol (EG)–NaOH solution without using poly(*N*-vinyl-2-pyrrolidone) (PVP) as a stabilizing agent revealed the difficulty in preparing fully homogenous bimetallic Ni/Pd alloy and preventing the formation of NiO on the surface of Ni nanoparticles. Shifted Ni and pure Pd metallic phases in the X-ray diffraction patterns and NiO related small peaks at 855.5 eV as well as Ni and Pd at 853.7 and 335.9 eV, respectively, in XPS spectra were observed. It was reported that even if two monolayers of NiO are formed on the Ni surface, the intensity of the Ni<sup>2+</sup> (2p) peak is greater than the Ni<sup>0</sup> (2p) peak [19]. Therefore, the extent of oxidation of Ni is not significant and the oxidation may be due to oxygen associated with EG absorbed on the Ni particles and hydroxide formation on the Ni surface during filtering and washing with water. The mixing of Pd salt with Ni salt was very effective to reduce the Ni<sup>2+</sup> ions with ethylene glycol because the solution showed very fast color change from yellow

to dark brown during refluxing. It was reported that the Ni<sup>2+</sup> ions are thought to be reduced at the surface of the Pd nanoparticles, presumably on the most catalytically active {1 1 1} surface [20].

Fig. 2 shows the TEM images and corresponding electron diffraction patterns of SWNTs and supported Ni catalysts. The particles essentially were monodispersed with an average diameter of 5.0–7.0 nm, consistent with the crystallite size of 5.6 nm calculated by calculated by TOPAS program from X-ray diffraction patterns. Five fringe patterns with plane distances of 3.13, 2.11, 1.83, 1.29, and 1.10 Å could be observed from Ni nanoparticle catalysts on SWNTs and four fringe patterns (nos. 2–5) except for the first pattern related to SWNTs were consistent with the indices (1 1 1), (2 0 0), (2 2 0), and (3 1 1) of pure face-centered cubic (fcc) nickel as shown in Fig. 2d.

### 3.2. Dehydrogenation behavior of the milled nanocrystalline composites of MgH<sub>2</sub> containing different catalysts

Fig. 3 shows DSC curves of the as received and as-milled samples with or without catalysts at a heating rate of 5 °C/min.

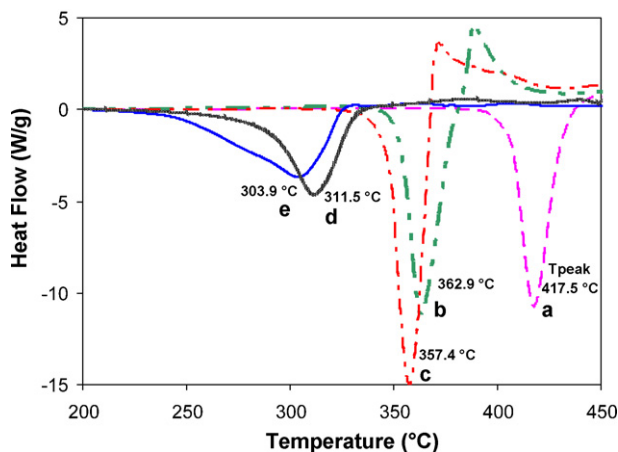


Fig. 3. DSC curves of (a) as-received  $\text{MgH}_2$ , (b) 18 h milled  $\text{MgH}_2$ , (c)  $\text{MgH}_2$ -BCN composite, (d)  $\text{MgH}_2$ -BCN-Ni/Pd(=2/1)/SWNTs composite and (e)  $\text{MgH}_2$ -BCN-Ni/Pd(=10/1)/SWNTs composite, at a heating rate of  $5^\circ\text{C}/\text{min}$ .

The endothermic peaks correspond to the decomposition of the hydrides phases. The nanostructured  $\text{MgH}_2$  milled for 18 h has a hydrogen desorption peak around  $363^\circ\text{C}$ , which is much lower than that of as received  $\text{MgH}_2$  ( $417.5^\circ\text{C}$ ). Thus, the reduction of crystallite size was very effective to decrease the decomposition temperature. The BCN doping to milled  $\text{MgH}_2$  further decreased the decomposition temperature and increased the heat flow in comparison to non-catalyzed  $\text{MgH}_2$ , potentially resulting in the increase of the enthalpies of formation. The additional milling of the mixture of 2 wt.% of BCN and milled  $\text{MgH}_2$  may cause the formation of Ba and Ca hydrides or hydroxides or  $(\text{Mg}, \text{M})\text{H}_x$  ( $\text{M} = \text{Ba}, \text{Ca}$ ) at the interface which can act as the enhanced path for hydrogen diffusion or active sites for hydrogen dissociation and recombination. However, the enthalpies of formation of  $\text{BaH}_2$  and  $\text{CaH}_2$  are 86 and 94 kJ/mol  $\text{H}_2$ , respectively, and higher than that of  $\text{MgH}_2$  (71 kJ/mol  $\text{H}_2$ ) [21]. In addition, the decomposition temperatures of  $\text{BaH}_2$  and  $\text{CaH}_2$  are 675 and  $600^\circ\text{C}$ , respectively, and much higher than that of  $\text{MgH}_2$  ( $327^\circ\text{C}$ ) [22]. There are many ternary hydrides such as  $\text{Ba}_2\text{MgH}_6$ ,  $\text{BaMgH}_4$ ,  $\text{Ba}_6\text{Mg}_7\text{H}_{26}$ ,  $\text{Ba}_2\text{Mg}_3\text{H}_{10}$ , and  $\text{Ca}_4\text{Mg}_3\text{H}_{14}$  that can be formed at the interface and have undefined values of the decomposition temperature and enthalpies of formation. Therefore, it is very difficult to determine the interfacial phases that cannot be detected by X-ray diffraction analysis. The kinetics of hydrogen sorption should be investigated for evaluating the effectiveness of BCN doping and is described in the next section. The further addition of 2 wt.% of Ni-Pd nanocatalysts on SWNTs into BCN-doped  $\text{MgH}_2$  decreased the peak decomposition temperature to about  $310^\circ\text{C}$  and broadened DSC profile in the temperature range from 340 to  $220^\circ\text{C}$ . The Ni-rich nanocatalyst-added  $\text{MgH}_2$  composite exhibited the most superior catalytic effect among all composites tested in this work and asymmetrical endothermic peaks having the low temperature peak related to the desorption from  $\gamma$ - $\text{MgH}_2$  and some amount of  $\beta$ - $\text{MgH}_2$  [23].

Fig. 4 shows Kissinger plot of the hydrogen desorption reaction for catalyzed  $\text{MgH}_2$  samples at various heating rates ( $\beta = 1, 5, 10,$  and  $20^\circ\text{C}/\text{min}$ ). The apparent activation energy for hydro-

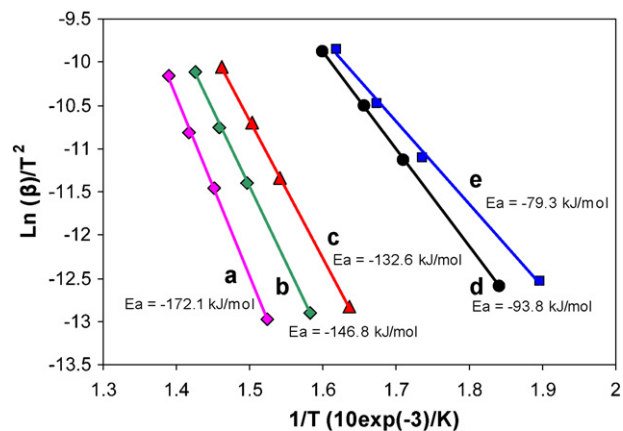


Fig. 4. Kissinger plots of the hydrogen desorption reaction of (a) as-received  $\text{MgH}_2$ , (b) 18 h milled  $\text{MgH}_2$ , (c)  $\text{MgH}_2$ -BCN composite, (d)  $\text{MgH}_2$ -BCN-Ni/Pd(=2/1)/SWNTs composite and (e)  $\text{MgH}_2$ -BCN-Ni/Pd(=10/1)/SWNTs composite at various heating rates ( $\beta = 1, 5, 10,$  and  $20^\circ\text{C}/\text{min}$ ).

gen desorption can be estimated by the Kissinger method [24] from DSC curves using the following equation:

$$\ln\left(\frac{\beta}{T_p^2}\right) = -\frac{E_a}{RT_p} + \alpha \quad (1)$$

where  $\beta$  is the heating rate,  $T_p$  the peak temperature,  $E_a$  the apparent activation energy,  $R$  the gas constant, and  $\alpha$  is the linear constant.

From the slope of these straight lines, the activation energies of as received  $\text{MgH}_2$  and 18 h milled  $\text{MgH}_2$  were estimated to be 172.1 and 146.8 kJ/mol, respectively, similar to the reported values (156 and 144 kJ/mol) [25,5]. Even though BCN catalyst was very effective to enhance desorption kinetics at  $300^\circ\text{C}$  [9,10], Ni/Pd metallic catalysts were much effective to enhance sorption kinetics at lower temperature according to DSC data. Ni-rich nanocatalyst-added  $\text{MgH}_2$  composite exhibited the low activation energy of 79.3 kJ/mol, corresponding to the reported values (88.1 and 74 kJ/mol) [2,5].

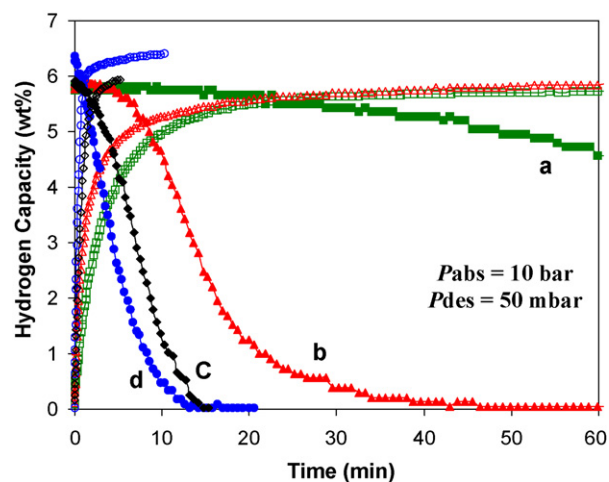


Fig. 5. Hydrogen absorption and desorption curves of (a) 18 h milled  $\text{MgH}_2$ , (b)  $\text{MgH}_2$ -BCN composite, (c)  $\text{MgH}_2$ -BCN-Ni/Pd(=2/1)/SWNTs composite and (d)  $\text{MgH}_2$ -BCN-Ni/Pd(=10/1)/SWNTs composite at  $300^\circ\text{C}$ .

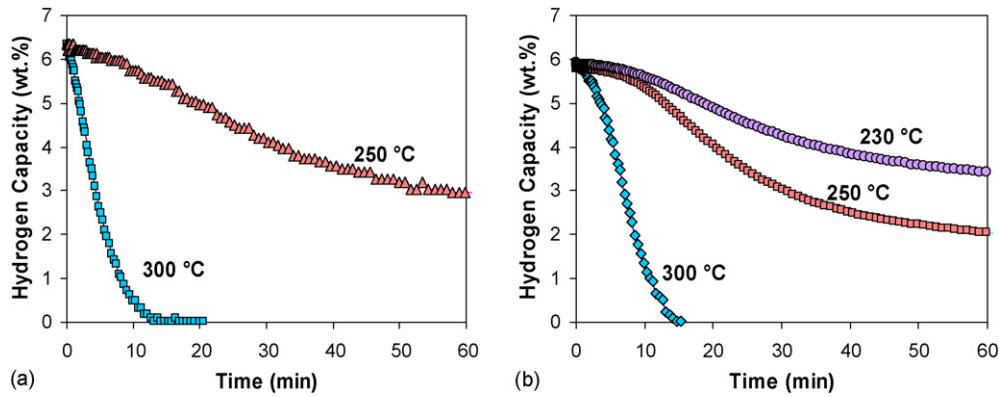


Fig. 6. Hydrogen desorption curves of (a)  $\text{MgH}_2\text{-BCN-Ni/Pd}(=10/1)/\text{SWNTs}$  composite, and (b)  $\text{MgH}_2\text{-BCN-Ni/Pd}(=2/1)/\text{SWNTs}$  composite under an initial hydrogen pressure of 50 mbar at different temperatures.

### 3.3. Hydrogen sorption properties

Fig. 5 shows the hydrogen absorption and desorption curves of the composites. The Ni-rich ( $\text{Ni/Pd} = 10/1$ ) nanocatalyst-added  $\text{MgH}_2$  composite exhibited the best absorption and desorption kinetics at  $300^\circ\text{C}$ , corresponding to the apparent activation energies of hydrogen desorption determined by DSC. Ni has a comparatively high 3d orbital occupancy. Therefore, occupied state is dominant with respect to the 3d orbital. This largely contributes to the back-donation of the electrons to the antibonding orbitals of  $\text{MgH}_2$ , resulting in the easier Mg–H dissociation [26].

Fig. 6 shows the hydrogen desorption curves of (a)  $\text{MgH}_2\text{-BCN-Ni/Pd}(=10/1)/\text{SWNTs}$  composite, and (b)  $\text{MgH}_2\text{-BCN-Ni/Pd}(=2/1)/\text{SWNTs}$  composite under an initial hydrogen pressure of 50 mbar at 230, 250 and  $300^\circ\text{C}$ . It can be seen that both of catalysts are not sufficient to provide fast kinetics and high hydrogen capacity at 230 and  $250^\circ\text{C}$ , even if DSC data of catalyzed  $\text{MgH}_2$  are quite promising to enhance sorption behavior at low temperature. Therefore, the effect of the concentration of catalysts on enhancing desorption kinetics at low temperature should be further investigated.

The PCI (pressure–composition–isotherms) curves at  $300^\circ\text{C}$  for nanostructured  $\text{MgH}_2$  composites with different catalysts

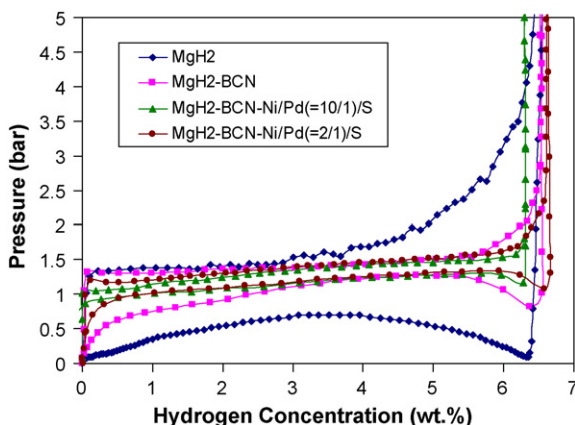


Fig. 7. PCI curves at  $300^\circ\text{C}$  for nanostructured  $\text{MgH}_2$  composites with different catalysts.

are shown in Fig. 7. The various catalyst-containing  $\text{MgH}_2$  composites exhibited high maximum hydrogen absorption capacities,  $(\text{H/M})_{\text{max}}$  in the range of 6.3–6.7 wt.%. The equilibrium pressures of H-desorption and reversible hydrogen absorption–desorption capacities for catalyzed  $\text{MgH}_2$  increased significantly in comparison to non-catalyzed  $\text{MgH}_2$ . The hysteresis,  $\ln(P_{\text{abs}}/P_{\text{des}})$ , of catalyzed  $\text{MgH}_2$  during hydrogen absorption and desorption was much smaller than non-catalyzed  $\text{MgH}_2$  due to the decreased mechanical stress between the metal and the hydride phases or the reduced kinetic constraints during the measurement [27].

### 4. Conclusions

Nanocrystalline  $\text{MgH}_2$  composites co-catalyzed with  $\text{Ba}_3(\text{Ca}_{1+x}\text{Nb}_{2-x})\text{O}_{9-\delta}$  (BCN) proton conductive ceramics and nanoparticle bimetallic catalyst of Ni/Pd dispersed on single wall carbon nanotubes (SWNTs) support have been successfully prepared by a consecutive combination of Pechini process, novel polyol method, and three step high energy milling. The apparent activation energies for the hydrogen desorption of  $\text{MgH}_2$  nanocomposites with or without catalysts were determined by the Kissinger method from DSC curves. The Ni-rich ( $\text{Ni/Pd} = 10/1$ ) nanocatalyst-added  $\text{MgH}_2$  composite exhibited the fastest absorption and desorption kinetics at  $300^\circ\text{C}$ , but 2 wt.% addition of SWNTs-supported Ni/Pd catalysts was not enough to provide fast kinetics and high hydrogen capacity at 230 and  $250^\circ\text{C}$ . The maximum hydrogen absorption capacities of nanostructured  $\text{MgH}_2$  composites co-catalyzed with BCN and bimetallic supported catalysts,  $(\text{H/M})_{\text{max}}$  in the range of 6.3–6.7 wt.% were obtained by PCI (pressure–composition–isotherms) curves at  $300^\circ\text{C}$ . The nanostructured Mg composites co-catalyzed with BCN and bimetallic supported catalysts exhibited the significant enhancement of hydrogen desorption kinetics at 230– $300^\circ\text{C}$  in comparison to either non-catalyzed  $\text{MgH}_2$  or the nanocomposite of  $\text{MgH}_2$  catalyzed with BCN.

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